

# Predicting and Improving the Performance of a Bagless Vacuum Cleaner using CFD

**Francisco Campos** | [f.campos@iconcfd.com](mailto:f.campos@iconcfd.com)

*3<sup>rd</sup> ANSA &  $\mu$ ETA International Conference 2009*

Mr. Jim Ferguson

Mr. John Kidd

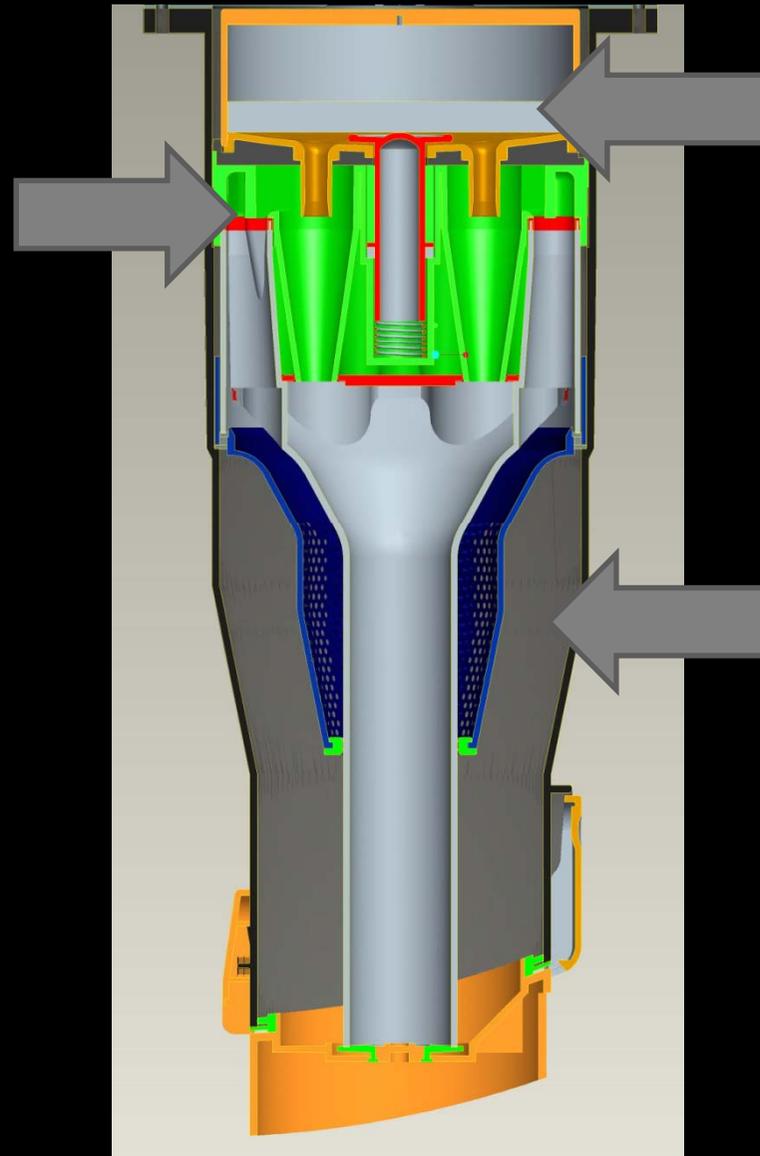
Mr. John Semple

Dr. David Sykes



- ❖ Bagless Vacuum Cleaner Technology
- ❖ Project Motivations
- ❖ CFD Methodology
- ❖ CFD Work Summary
  - 2<sup>nd</sup> Stage Cyclone Optimisation
  - Baseline Geometry
  - Optimised Geometry
- ❖ Conclusions

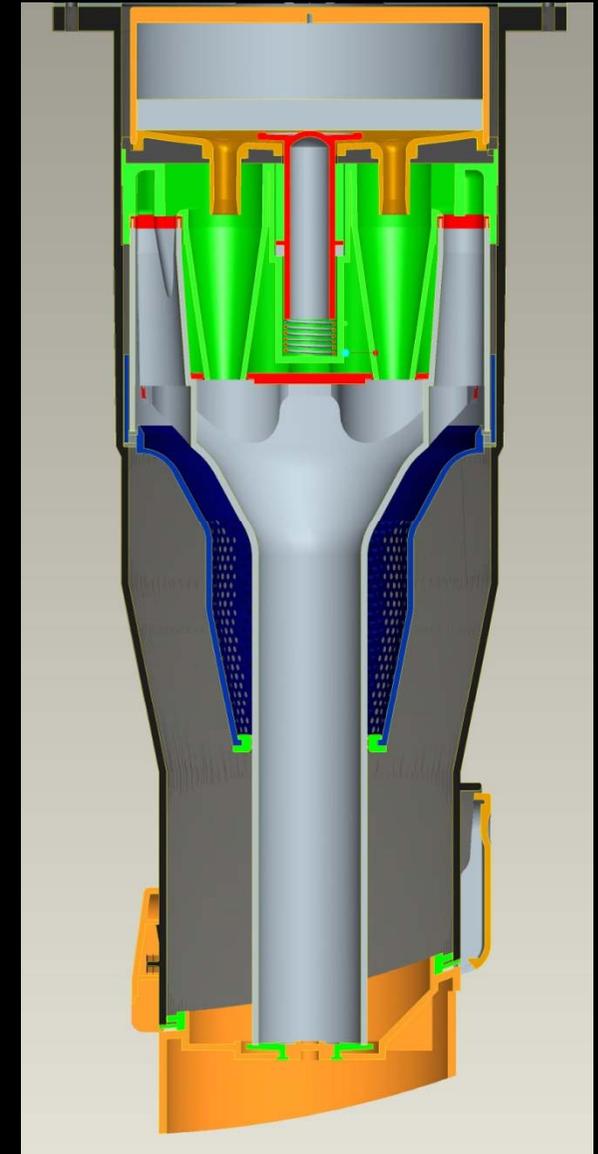
2<sup>nd</sup> Separation Stage  
- 12 cyclones  
- Small particles



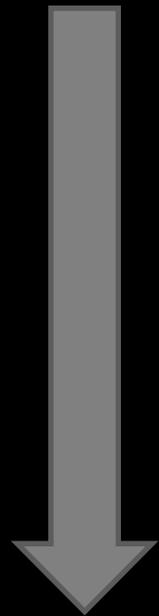
Filter  
- Micro particles

1<sup>st</sup> Separation Stage  
- Large solids

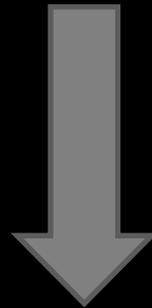
- ❖ Separation efficiency tested using Kaolin
- ❖ Can separation efficiency be improved beyond current values?
- ❖ Modify 2<sup>nd</sup> separation stage design?
- ❖ What happens at different operating flow rates?



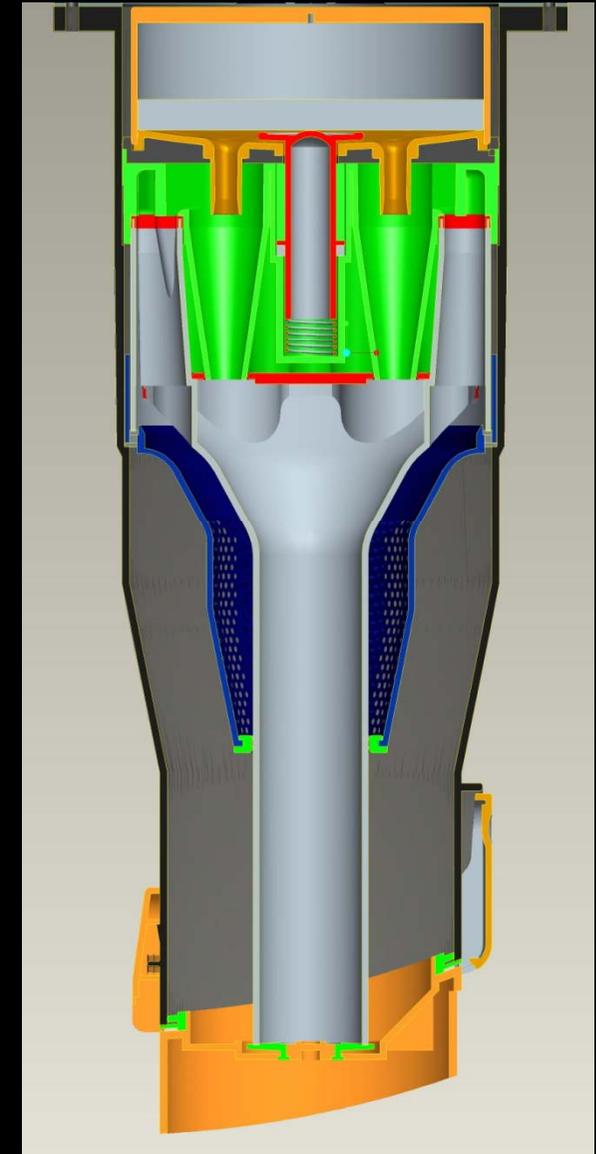
## Optimisation 2<sup>nd</sup> Separation Cyclone



CFD Baseline Design



CFD Modified Design

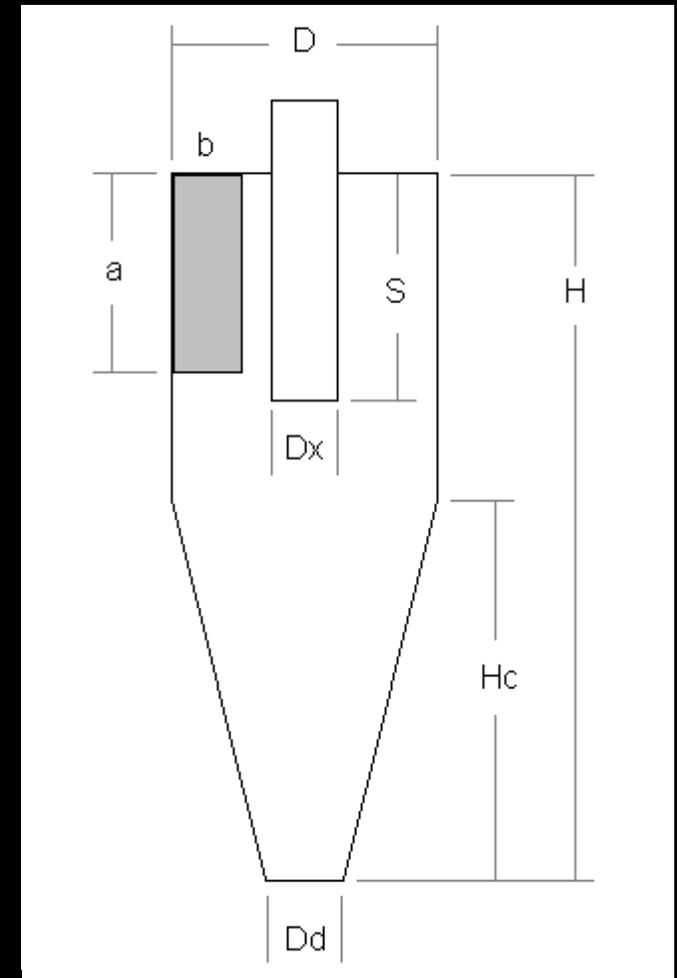


## Summary

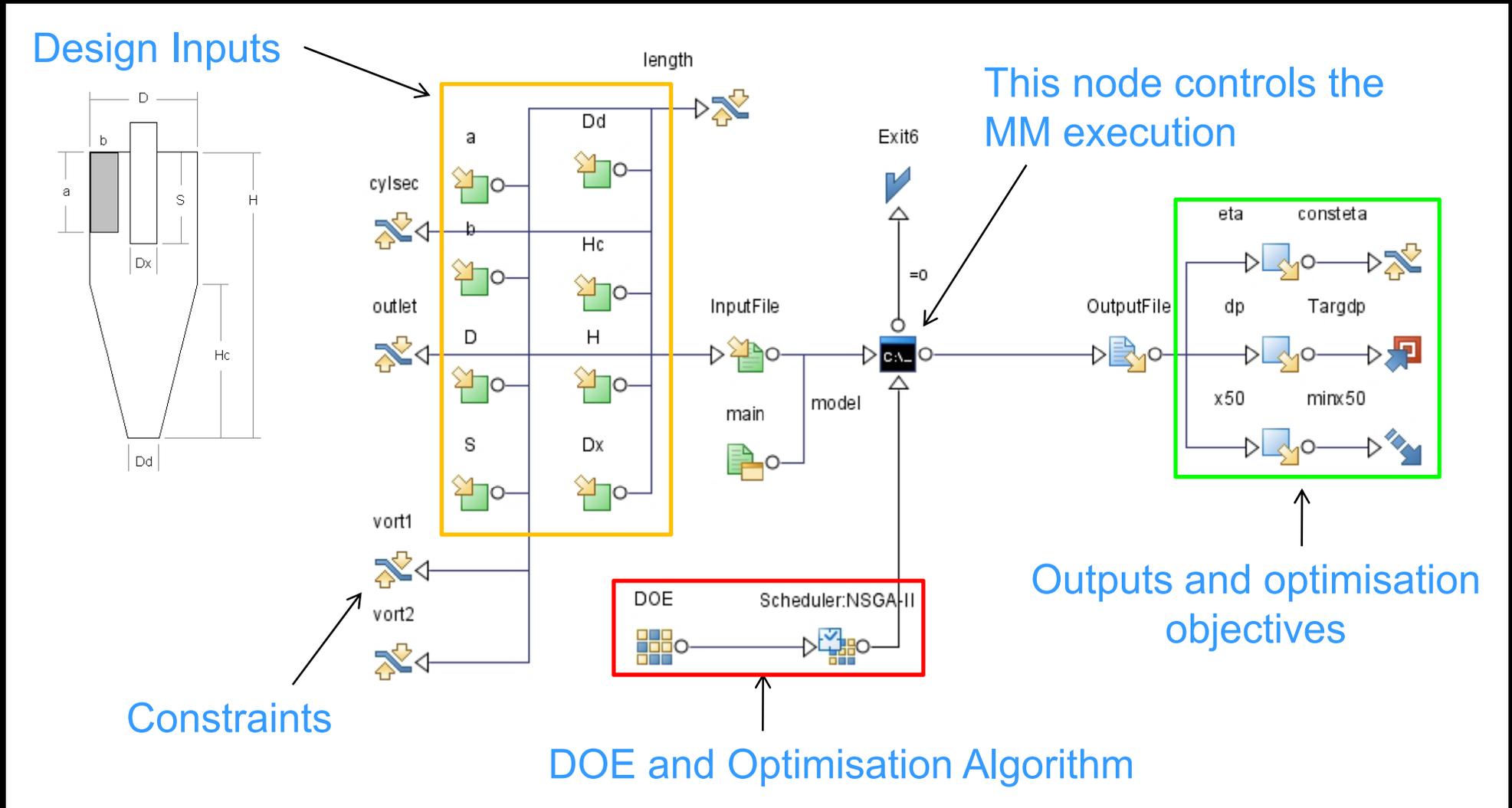
- ❖ Muschelknautz model (MM) implemented in Fortran
- ❖ modeFrontier → optimisation of individual 2<sup>nd</sup> stage separators cyclones using MM
  - Optimisation objectives:
    1. Minimise total pressure drop ( $\Delta p$ )
    2. Maximise separation efficiency ( $\eta_{max}$ )
  - 5792 feasible designs variations evaluated in mF → 72 initial designs from Sobol DOE followed by 100 NSGAI generations
- ❖ CFD tests performed using single cyclone parametric model for validation purposes

## Muschelknautz Model

- ❖ Semi-empirical model developed over 30 years to predict performance of cyclone separators across a wide range of sizes and applications.
- ❖ Model accounts for: wall roughness (due to material and collected solids); saltation or mass loading effects; particle size distribution.
- ❖ Model inputs → Geometric parameters  
Flow rates for air & solids  
Particle size distribution
- ❖ Outputs → Overall separation efficiency  
Total pressure loss  
x50 and Grade Efficiency Curve

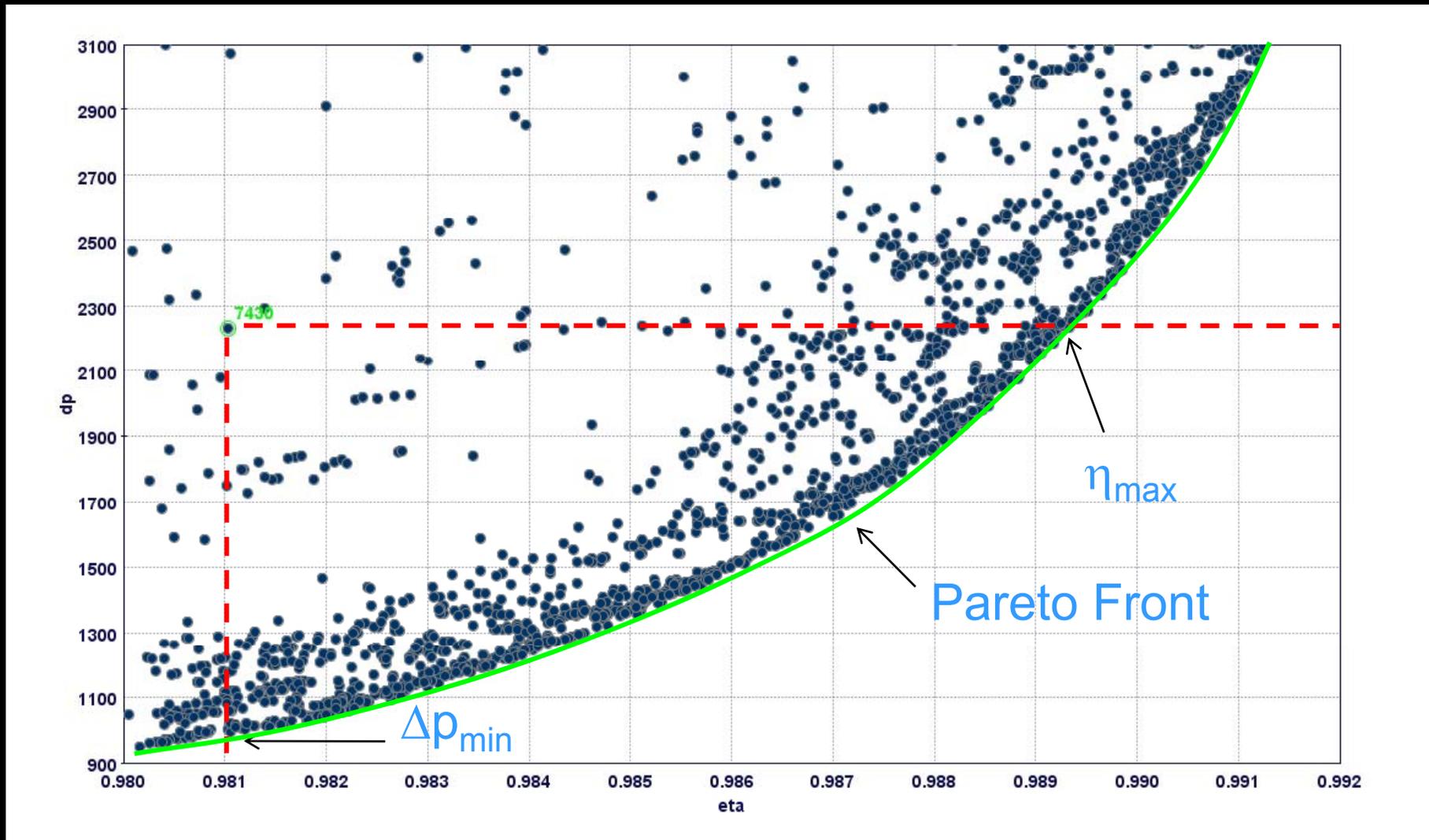


## mF Optimisation Workflow

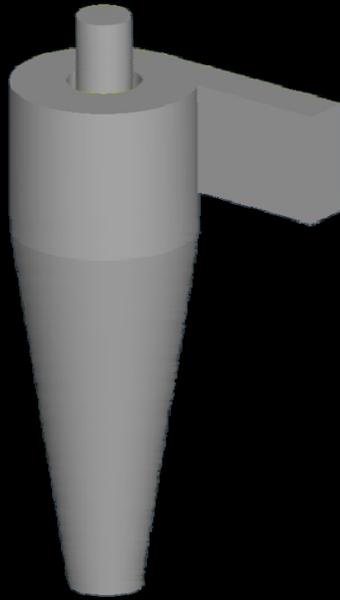


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## mF Optimisation Results: $\eta$ vs. $\Delta p$



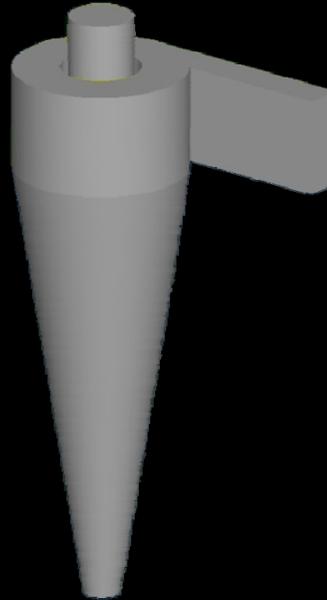
## mF Optimisation Results



Baseline

$$\eta = 98.10\%$$

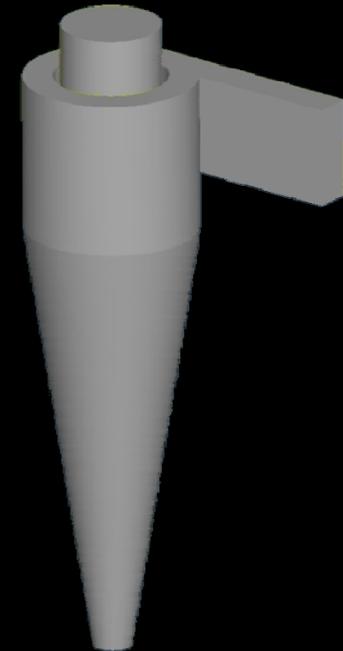
$$\Delta p_0 = 2232.9 \text{ Pa}$$



$\eta_{\max}$

$$\eta = 98.93\%$$

$$\Delta p_0 = 2236.8 \text{ Pa}$$



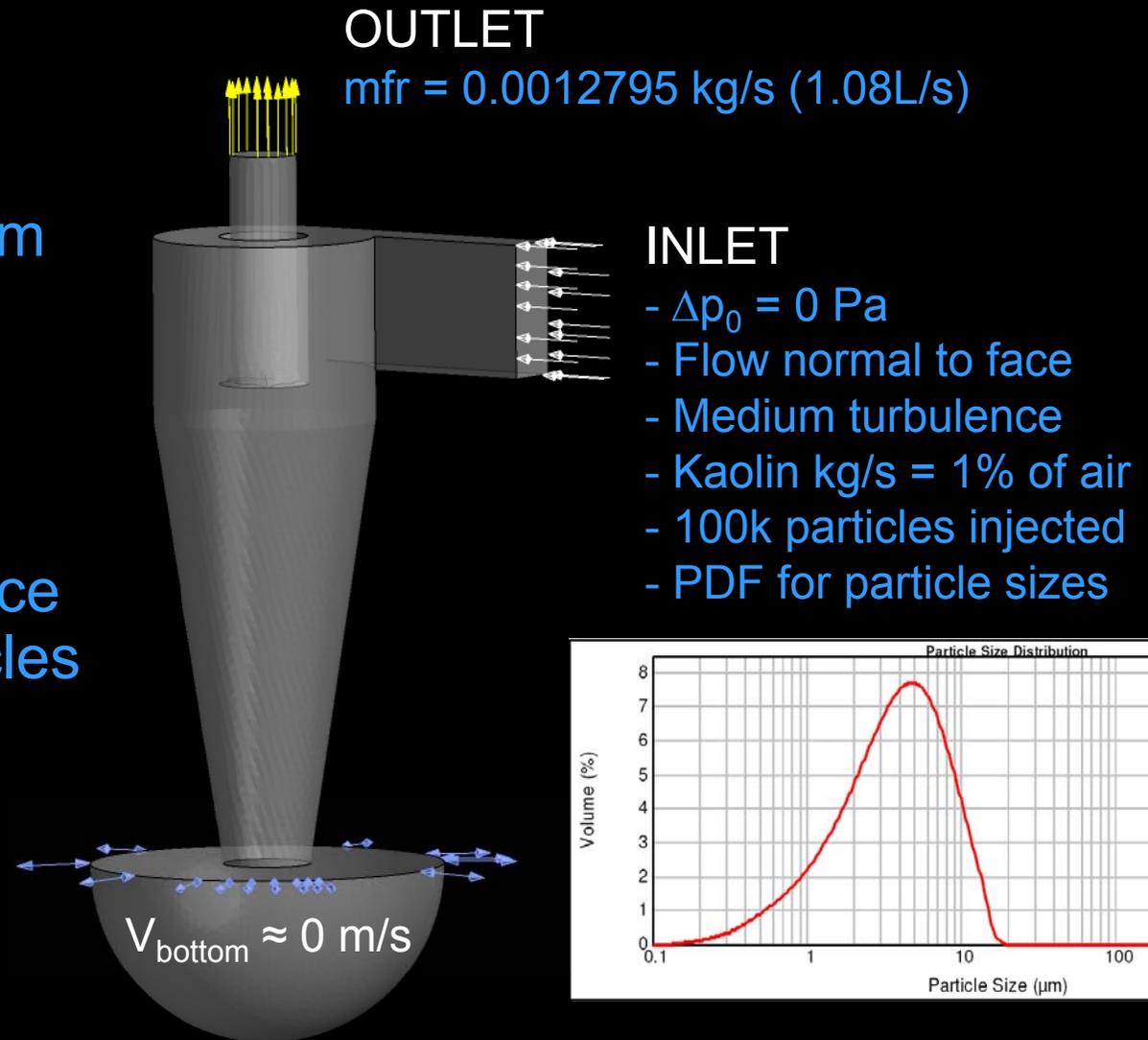
$\Delta p_{\min}$

$$\eta = 98.10\%$$

$$\Delta p_0 = 996.0 \text{ Pa}$$

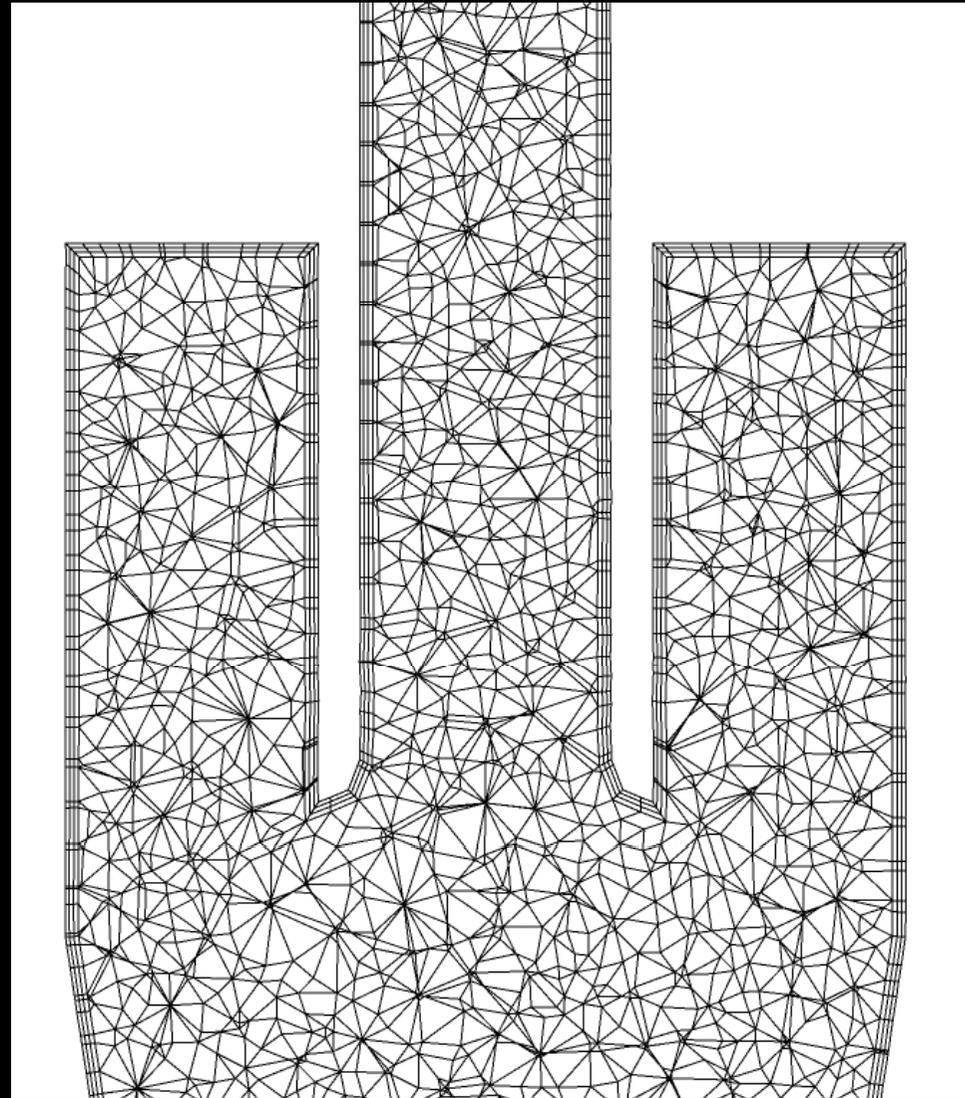
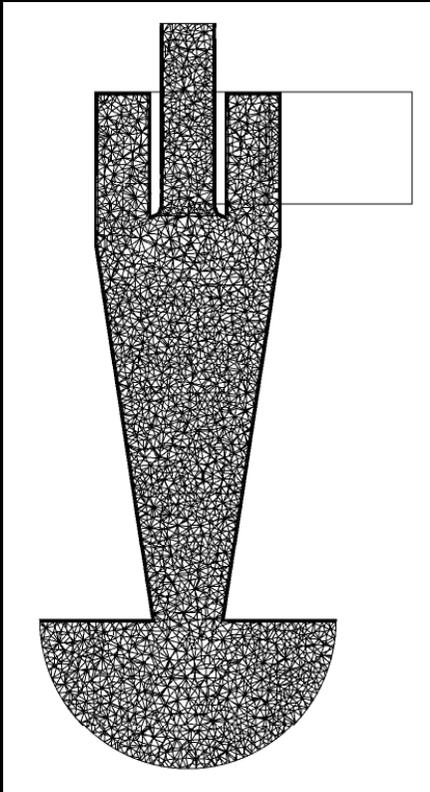
## CFD Validation Model: CFX

- ⌘ Steady-state flow
- ⌘ Air constant properties evaluated at 25°C and 1atm
- ⌘ Turbulence → BSL RSM
- ⌘ Uncoupled Lagrangian particle tracking
- ⌘ Gravity, drag and turbulence effects evaluated on particles
- ⌘ Particles do not stick or deposit at walls



## CFD Mesh: ANSA

- ⌘ CFD Mesh → 200k Cells
- ⌘ CFD mesh algorithms

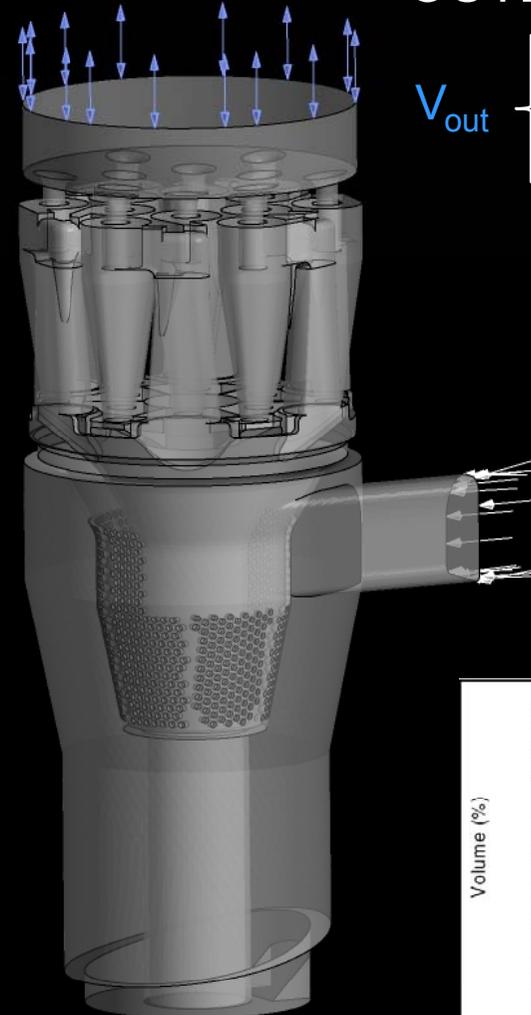


## MM Validation

		CFD Model	Muschelknautz Model
Baseline	$\eta$	98.73%	98.10%
	$\Delta p_0$	750.5 Pa	2232.9 Pa
$\eta_{\max}$	$\eta$	98.07%	98.93%
	$\Delta p_0$	1075.17 Pa	2236.8 Pa
$\Delta p_{\min}$	$\eta$	97.28%	98.10%
	$\Delta p_0$	650.15 Pa	996.0 Pa

## CFD Model: Ansys CFX

- ⌘ Steady-state flow
- ⌘ Air constant properties evaluated at 25°C and 1atm
- ⌘ Turbulence → BSL RSM
- ⌘ Uncoupled Lagrangian particle tracking
- ⌘ Gravity, drag and turbulence effects evaluated on particles
- ⌘ Particles do not stick or deposit at walls

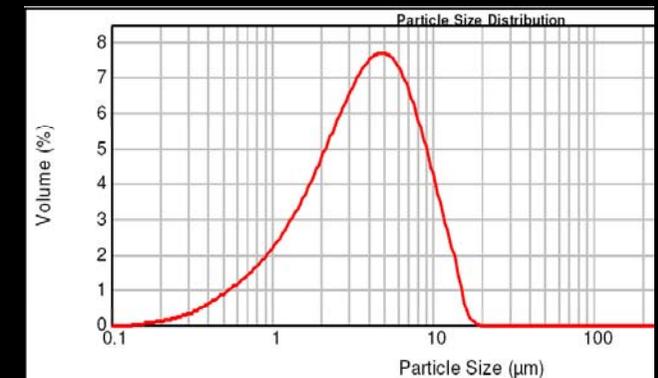


OUTLET

$$V_{out} \begin{cases} 1.179\text{m/s for } 13\text{L/s} \\ 1.904\text{m/s for } 21\text{L/s} \end{cases}$$

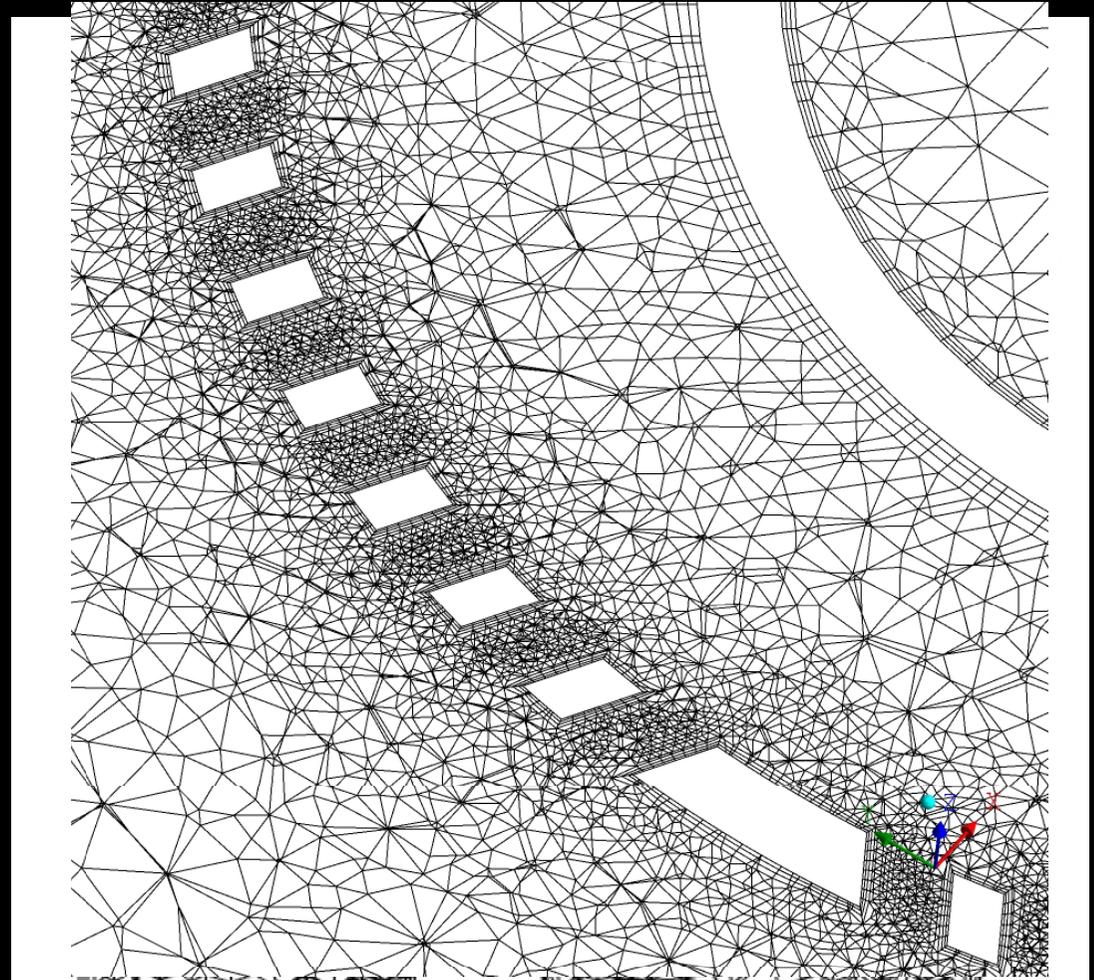
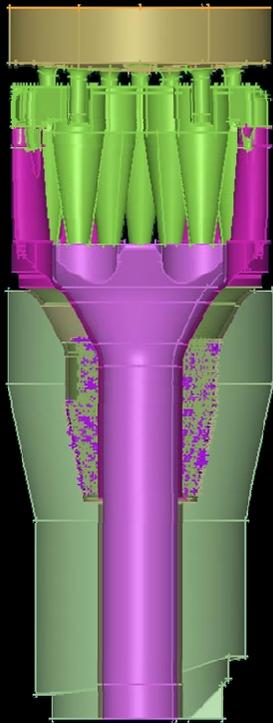
INLET

- $\Delta p_0 = 0 \text{ Pa}$
- Flow normal to face
- Medium turbulence
- Kaolin kg/s = 1% of air
- 100k particles injected
- PDF for particle sizes



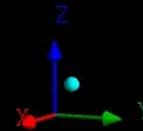
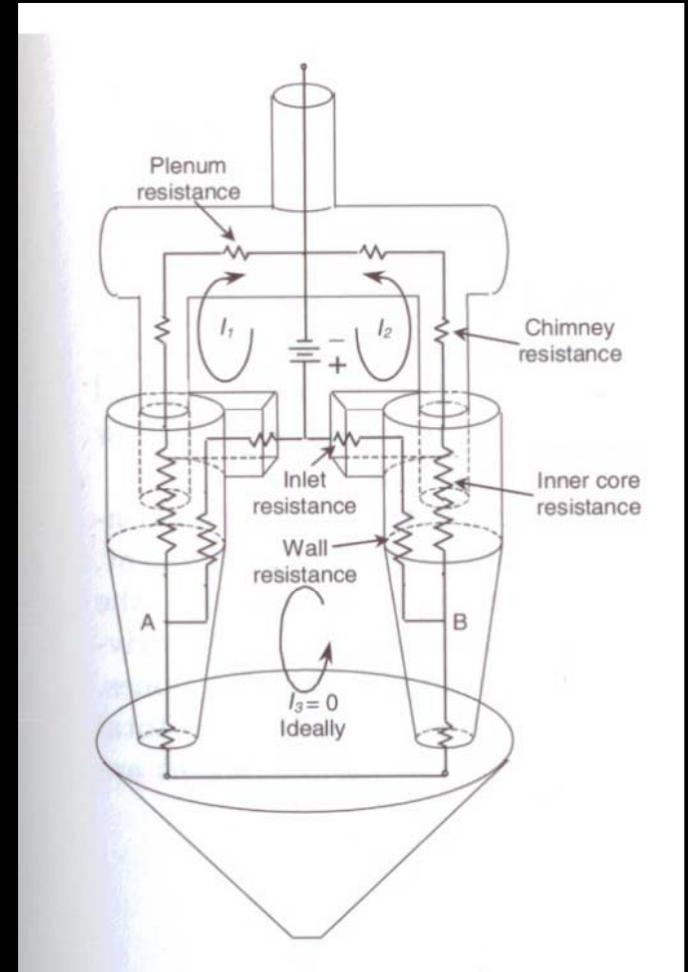
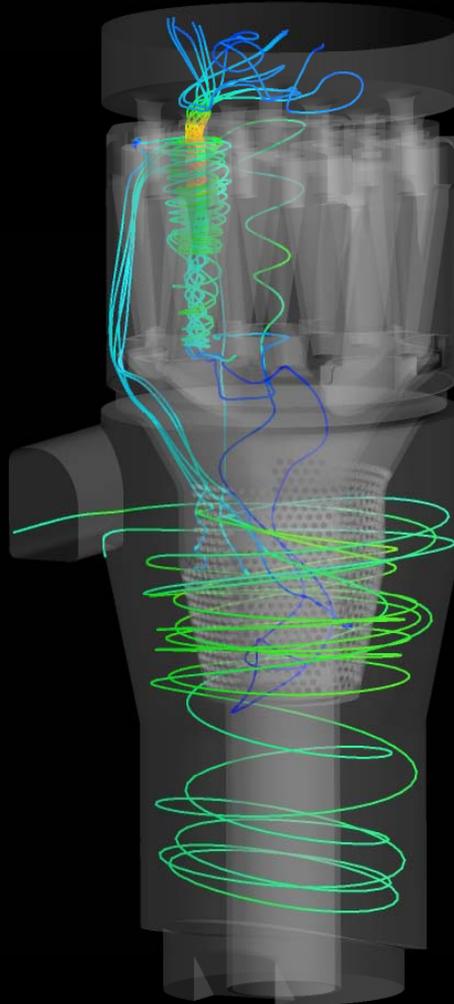
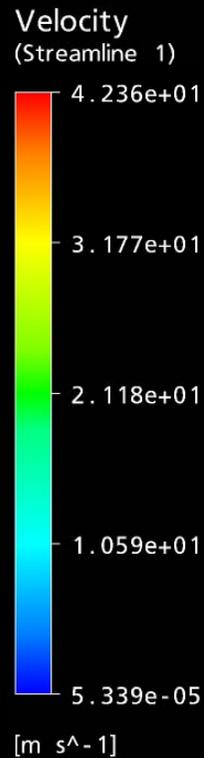
## CFD Mesh: ANSA

- ⌘ CAD preparation
- ⌘ CFD Mesh → 17.2M Cells
- ⌘ CFD mesh algorithms

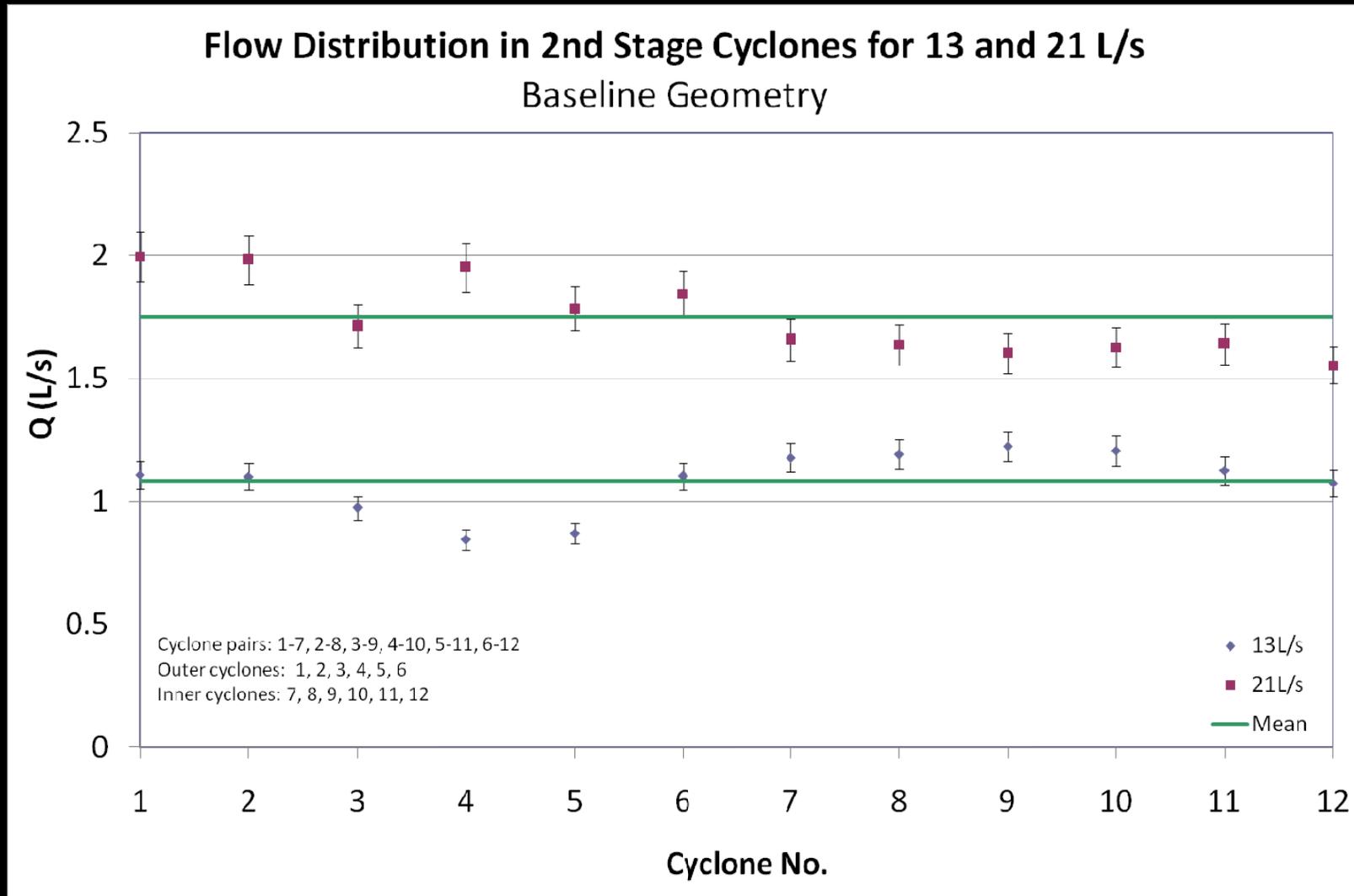


## Results: Hopper Cross Flow

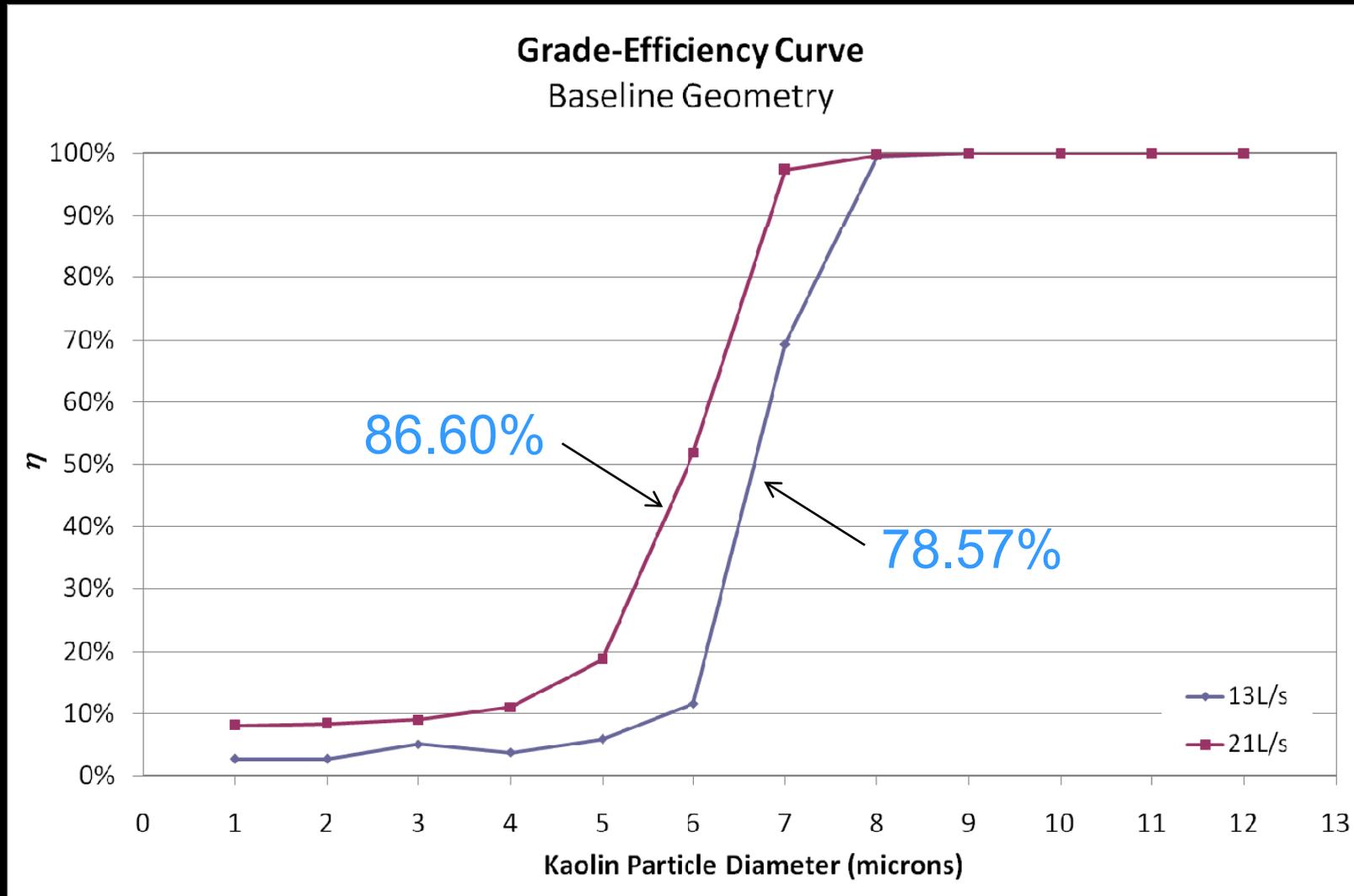
ANSYS

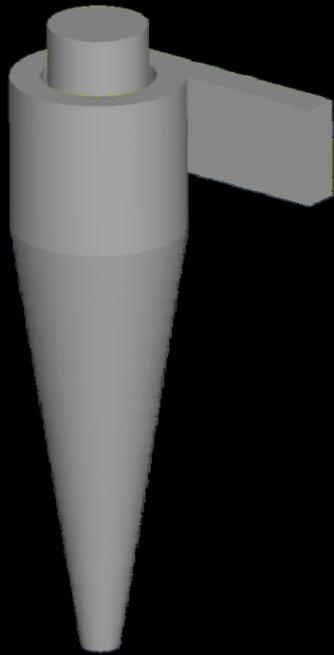


## Results: Flow Balance

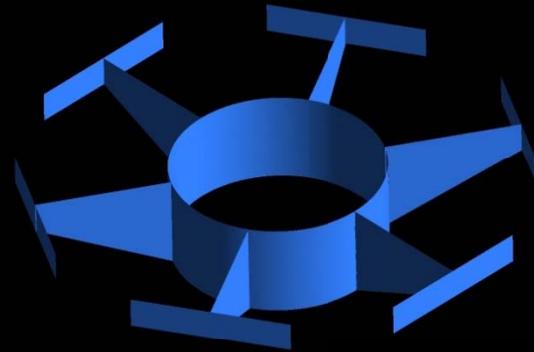


## Results: Separation Efficiency

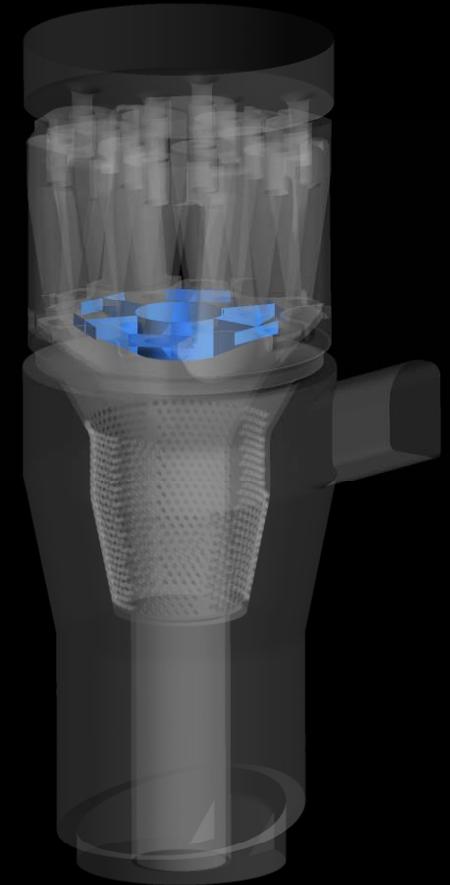




New 2<sup>nd</sup> Stage  
Cyclone

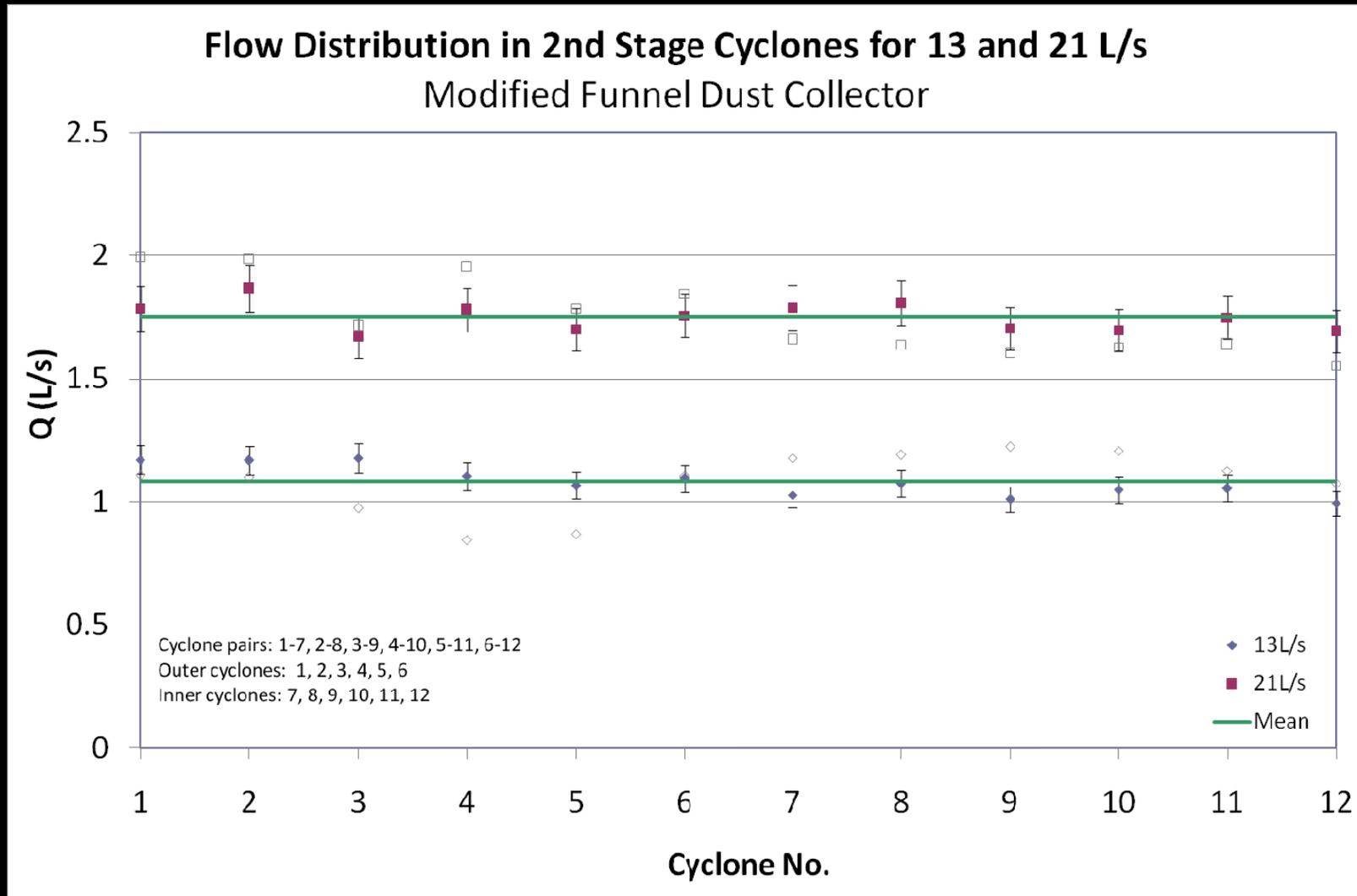


Corrective  
device for  
preventing  
hopper cross  
flows

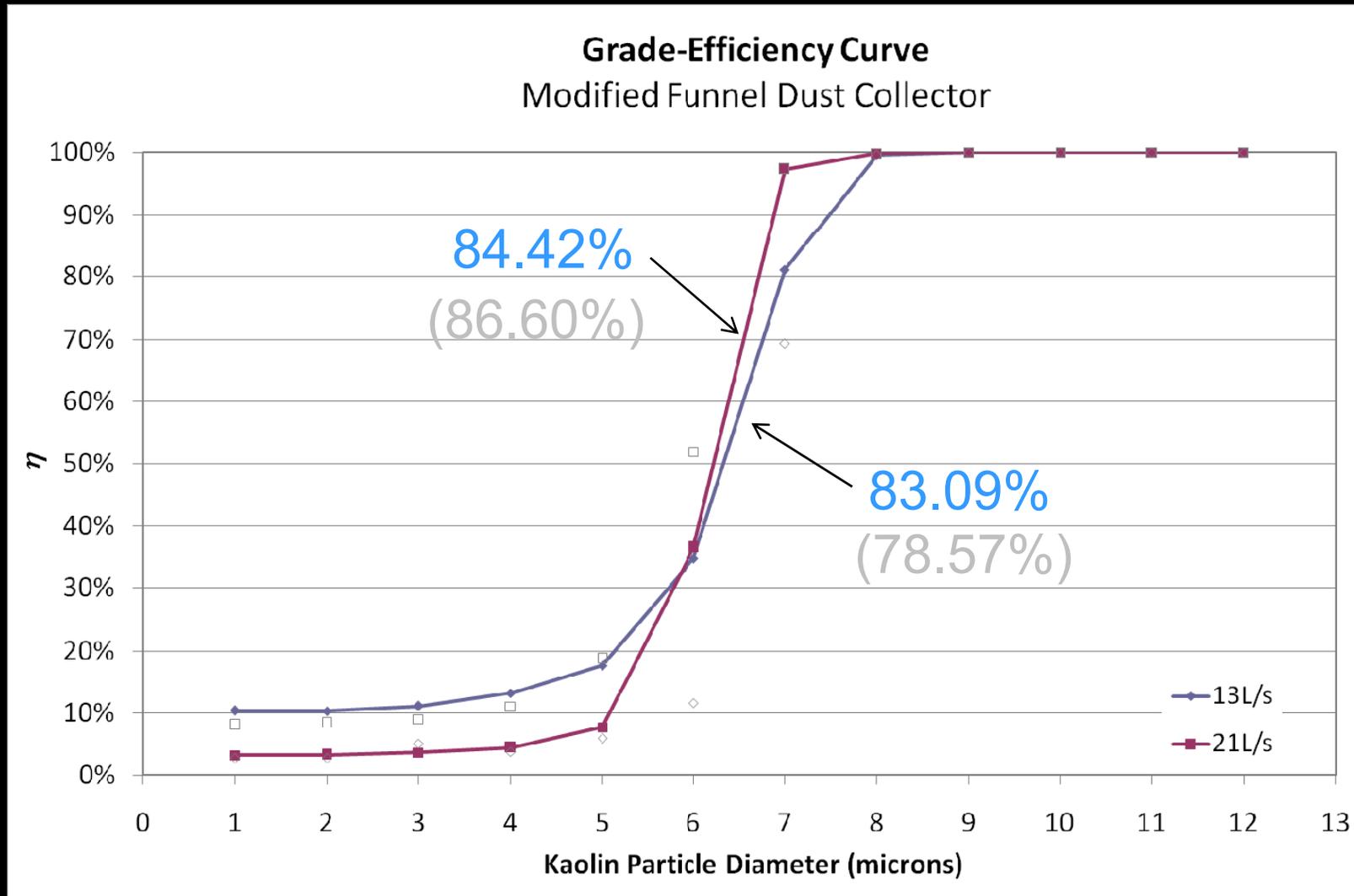


Modified  
Design

## Results: Flow Balance



## Results: Separation Efficiency



- ❖ A CFD methodology combining 1D analysis, modeFrontier, ANSA and CFX was developed to:
  - Estimate performance parameters
  - Understand existing/potential flow related phenomena not seen in experiments
  - Propose design modifications and verify their effects
- ❖ Benefits to Hoover Candy:
  - Ability to reduce prototyping
  - Ability to reduce testing
  - Better, cheaper and greener vacuum cleaners

Thank you for your attention



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